#### **Process Integration & Optimization Using Dynamic Systems Models**

Key words: <u>energy systems</u> integration & HiL simulation, dynamic energy <u>systems</u> <u>optimization</u>, predictive/safety critical <u>supervisory &</u> <u>resilient\_controls</u>, <u>smart energy grids/microgrids</u>

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#### **AIChE CAST Webinar Series**

January 14, 2014

#### **Objectives**

- Innovation
- Collaboration
- HiL demonstration

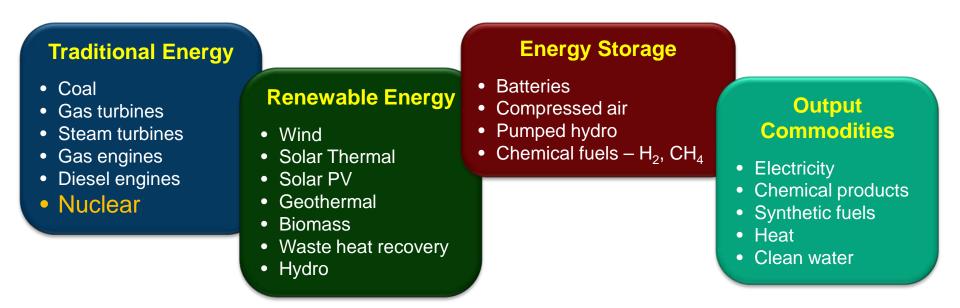




# Motivation

- Hybrid Energy Systems (HES)
- Modeling Issues
- Co-simulation Issues
- Optimization Issues
- Dynamic Analyses with Casual Models
- Dynamic Analyses with Acasual Models
- Optimization Studies with Acasual Models
- Conclusion

#### The world is powered by many energy sources...

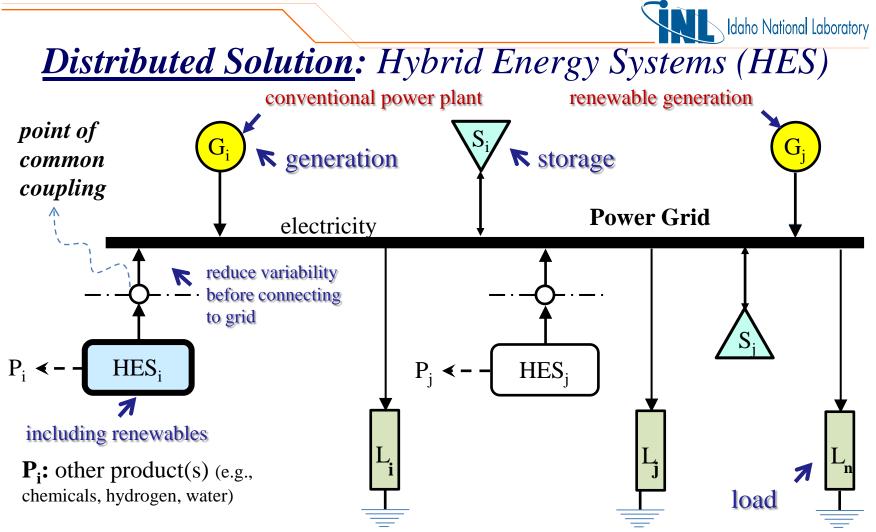


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[] ...are there COMBINATIONS or HYBRIDIZATIONS that are particularly attractive?
[] ...how are reliability and environmental stewardship affected by selected configurationS?
[] ...can nuclear energy complement or compensate for renewable energy build-out and emerging grid dynamics?

[] ...what is the role of next generation nuclear reactors?

[] ...how does system integration change energy storage needs?



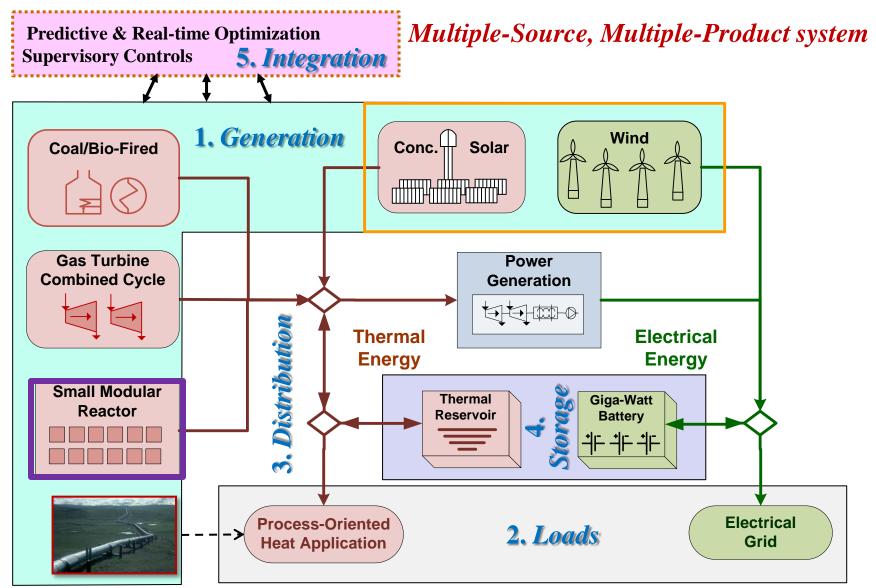
- Facilitate effective and efficient integration of clean & sustainable energy solutions;
- Enhance both **power & energy management**, in addition to reliability and **security**;
- Extended electrical & thermal options for variability management, thus reducing stress on power grid;
- Promote usage of carbon sources and reduce environmental impact;
- Leading to regional/nation-wide "energy grids";
- Support smooth integration of diverse energy sources and products within existing infrastructures;



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Hybrid Energy System (HES): A Multiple-Input, Multiple-Output (MIMO) system



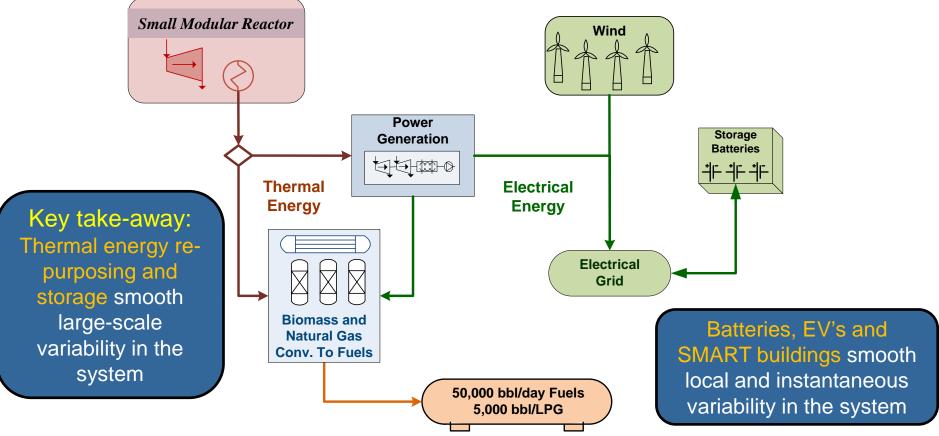
HYBRID (engine & battery)  $CARS \rightarrow HYBRID$  (nuc, ren, chem, grid) ENERGY SYSTEMS



## Keys to energy systems integration...

- Dynamic Integration
- Grid Stabilization
- Energy Storage

- Capital Efficiency
- Resource/system optimization
- Monitoring & Controls



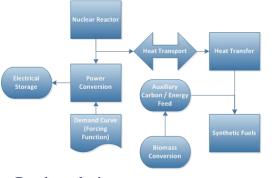


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#### Graded Approach to Identify, Design, Analyze, Test & **Optimize Advanced Energy Solutions**

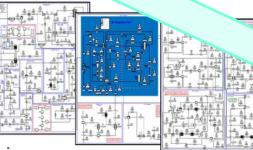
**Energy Solution Identification** based on Local/Global **Requirements & Constraints** 



• Batch analysis

• High-level requirements and resources analysis

Feasibility, Life-Cycle & Economic Assessment of **Identified Energy Solutions** 



• Steady-state analysis • Time-average analysis

Fuels

& Storage

"A system-centric approach to devise efficient, sustainable & resilient energy solutions"

> **Dynamic Analysis, Testing & Optimization** of Selected **Energy** Solutions



#### Energy Systems Laboratory

- Dynamic Performance/Cost Analysis
- Dynamic Integrated Equipment Analysis
- Multidimentional Co-optimization
- HiL testing & demonstration



Lifecycle Analyses, Hybrid System Design, Signal Processing & Visualization Advanced Controls



Systems Integration. Analyses, Optimization, Monitorina, Control



Feedstock Extraction & Processina

Heat exchanger/ heat circulation, Heat deposition Gas & liquids T/H Thermal Design

Energy Transfer

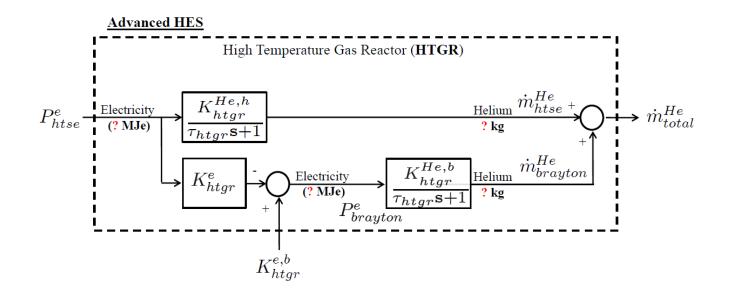
Energy Storage



Byproduct Management



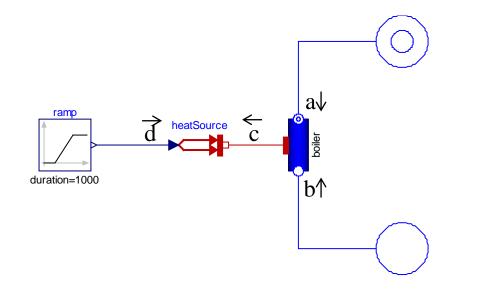
- Causal Modeling: Nuclear Reactor
  Electrical and thermal energy flows are modeled as signals modified by transfer functions.
- In causal modeling, energy flows are unidirectional (inputs and outputs must be specified).
- Transfer functions are derived from conducting mass and energy balance, and gains are calculated using efficiency and unit conversion values.



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## Acausal Modeling: Nuclear Reactor

- In contrast to causal (e.g., signal-based), acausal physics-based models solves governing equations for the actual physical phenomena in the system.
- In acausal models, equations are solved without regard for whether variables are inputs or outputs. Thus, equality relationships are interpreted as mathematical equalities as opposed to assignments.



Heat source:  $-\dot{Q}_c = \dot{Q}_d \left(1 + \alpha \left(T - T_{ref}\right)\right)$ Laminar flow:  $\Delta P = -\rho g \Delta z + \Delta P_{nominal} \frac{\dot{m}}{\dot{m}_{nominal}}$ Mass balance:

 $\dot{m}_a + \dot{m}_b = 0$ 

Energy balance:  $h_a \dot{m}_a + h_b \dot{m}_b = \dot{Q}_c$ 



#### **Requirements for Physical Systems Modeling, Co-simulation, Optimization**

#### **1.** Acausal/declarative: capable of solving problems of any structure

- No a priori need to identify givens (inputs) and unknowns (outputs)
- Formulation independent of actual boundary conditions
- Context-independent form, without caring about actual solution algorithm
- Facilitate model reusability
- 2. Multi-domain: effective integration of simulated models and physical systems from diverse disciplines
  - Complete integrated simulation including thermo-hydraulics, electrical, mechanical, and chemical dynamics of diverse energy conversion systems
  - Support <u>HiL</u> demonstrations
- **3. Open:** allow construction and/or modification of existing component modules to accommodate specific needs
- 4. **Dynamic & Hybrid:** emphasis on dynamic analysis to evaluate and accommodate issues related to flexible operation and variable generation
  - Dynamic performance and cost analysis, monitoring and controls, sensitivity, robustness, what-if analysis, optimization
  - Time-driven plus event-driven modeling "Selected Solution: Modelica"
- 5. Non-proprietary: Ease of collaboration through open licensing

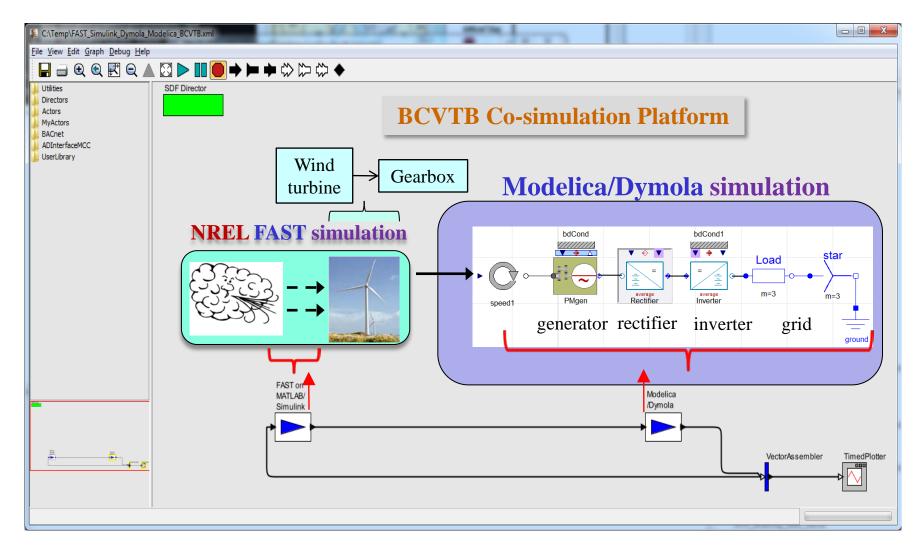


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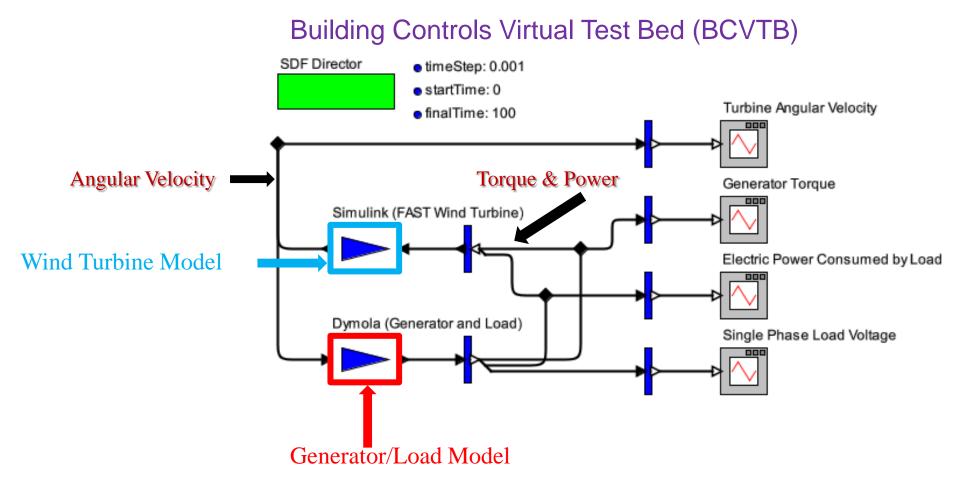
## **Co-Simulation of Wind Turbine & Generator Models (1)**

Shows from wind velocity to wind turbine, gearbox, generator, rectifier, inverter, grid/load



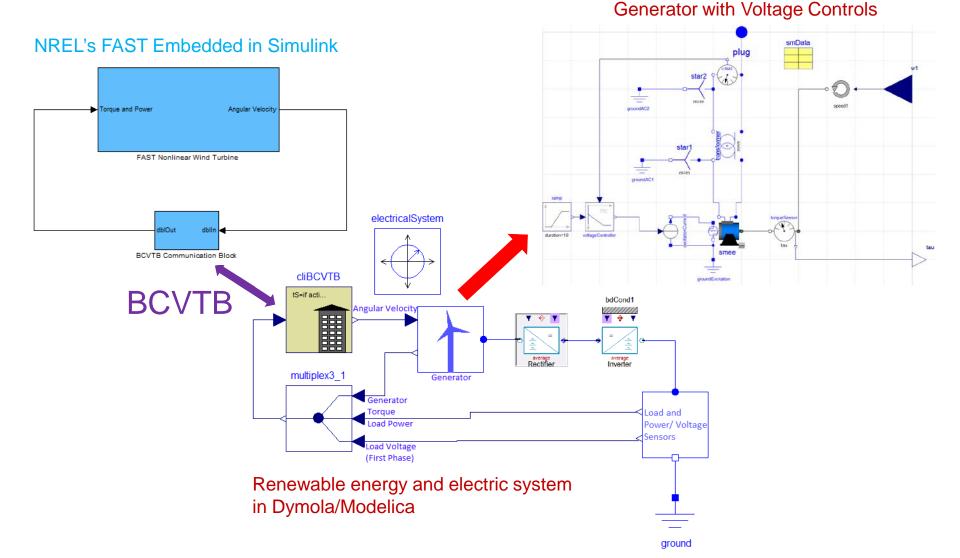


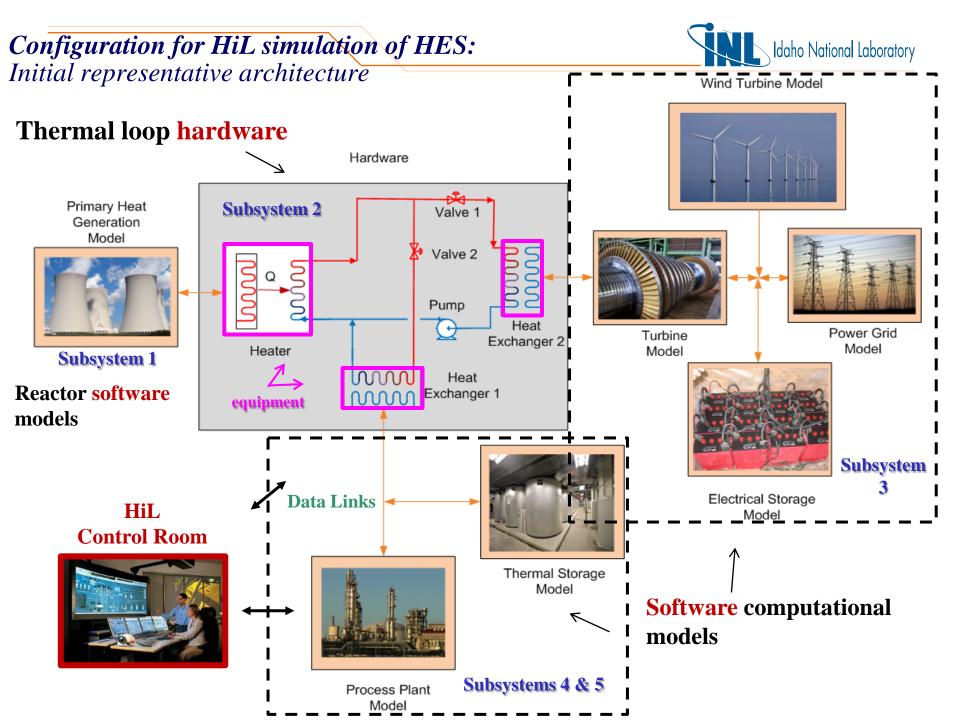
### **Co-Simulation of Wind Turbine & Generator Models (2)**





#### **Co-Simulation of Wind Turbine & Generator Models (3)**



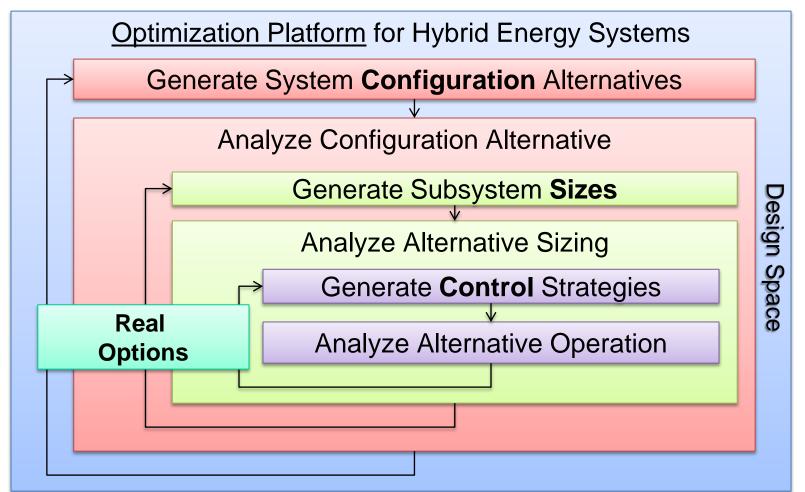




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#### **Optimization Challenge**

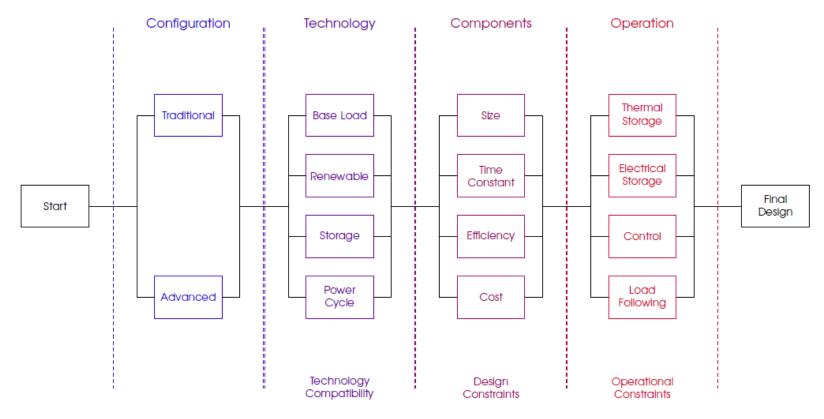


Optimizing one design variable without others does not guarantee an optimum and it is also inefficient and costly Maximize Utility over Design Space: configuration, sizing, control, real options



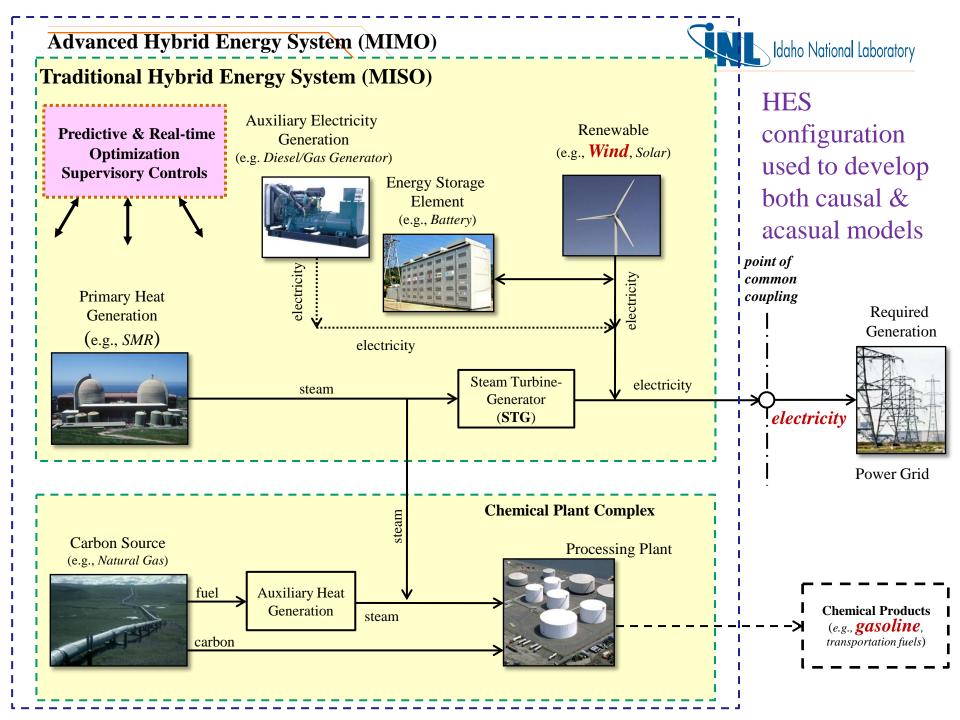
# **Current Architecture**

- Extending computational framework to consider:
  - more detailed models (physics-based);
  - alternative configurations and technologies;
  - operation and control of HES.
- A decision tree classifies design aspects into distinct layers:

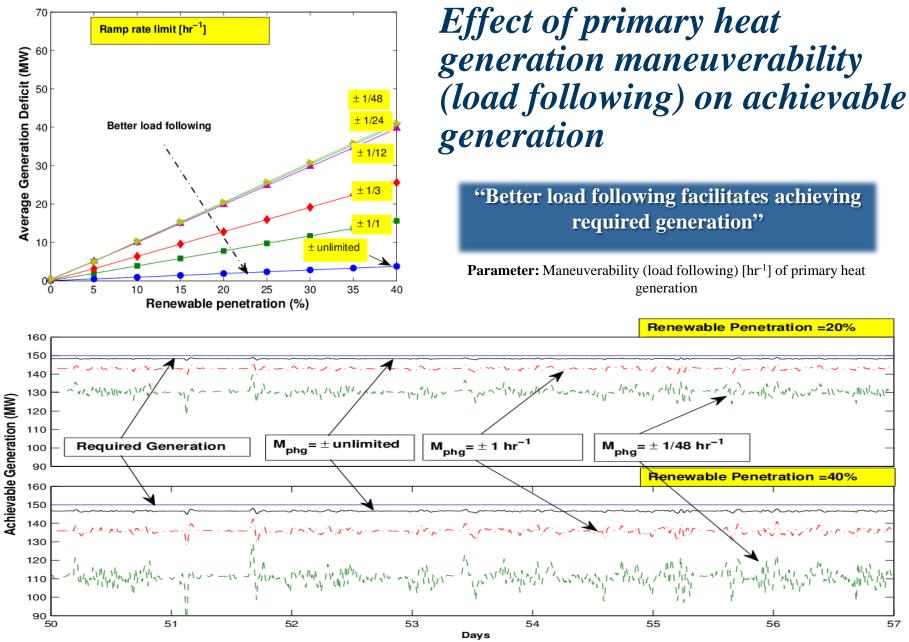




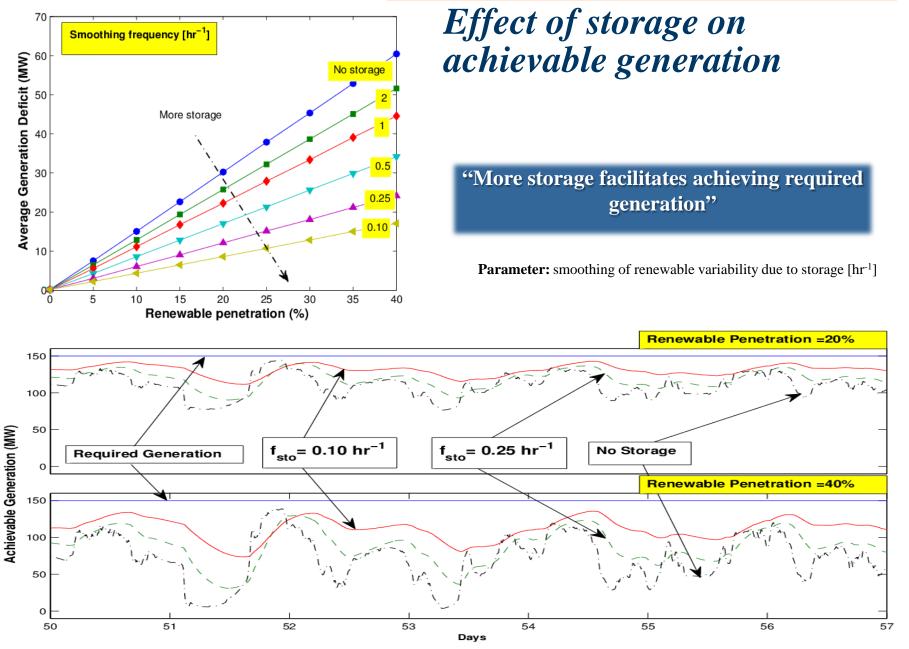
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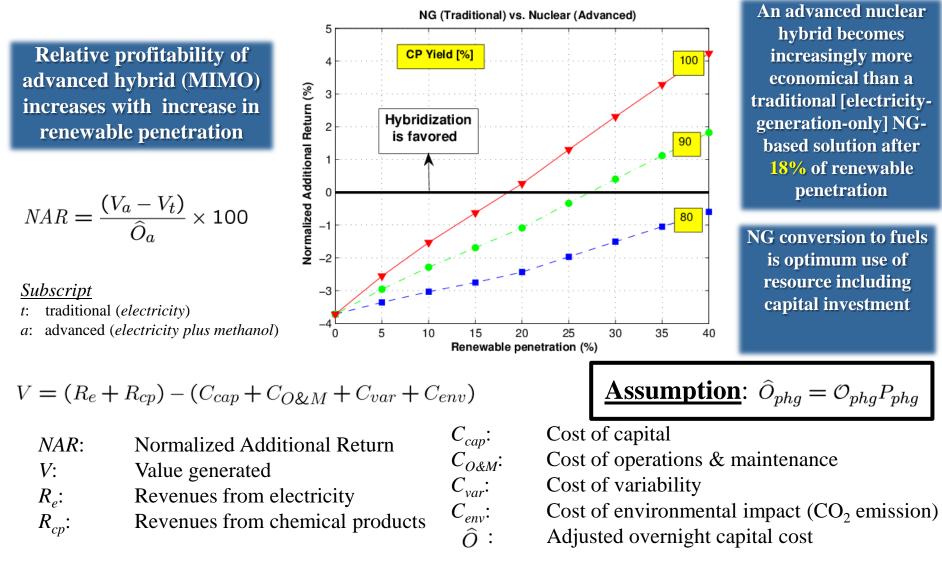








#### Traditional (electricity-only) NG-based HES vs. advanced (electricity-methanol) nuclear-based HES

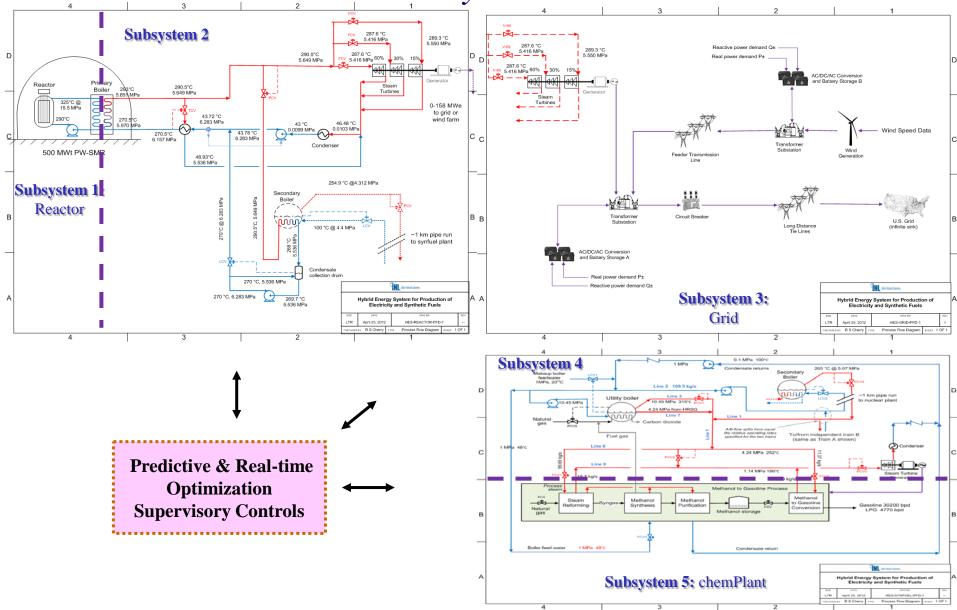




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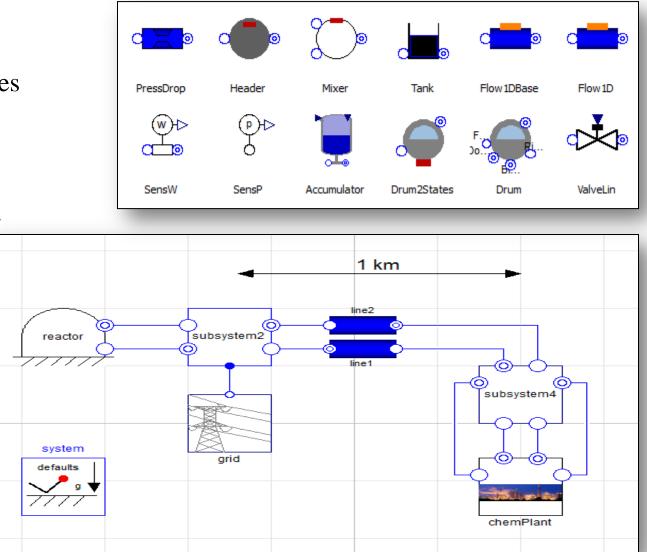
#### Illustrative HES: Nuclear Hybrid w/ Renewables





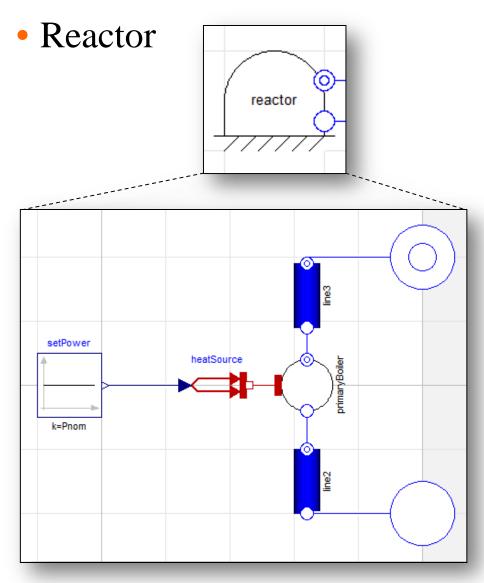
# **HES Computational M&S:** Overview

- Builds on
  - In-house libraries
  - Open-source libraries
- Five main subsystems
  - 1. Reactor
  - 2. Power generation (subsys2)
  - 3. Electrical grid
  - 4. Steam control (subsys4)
  - 5. Chemical plant

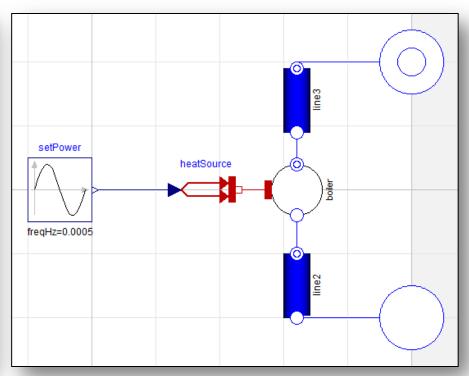




### Reactor

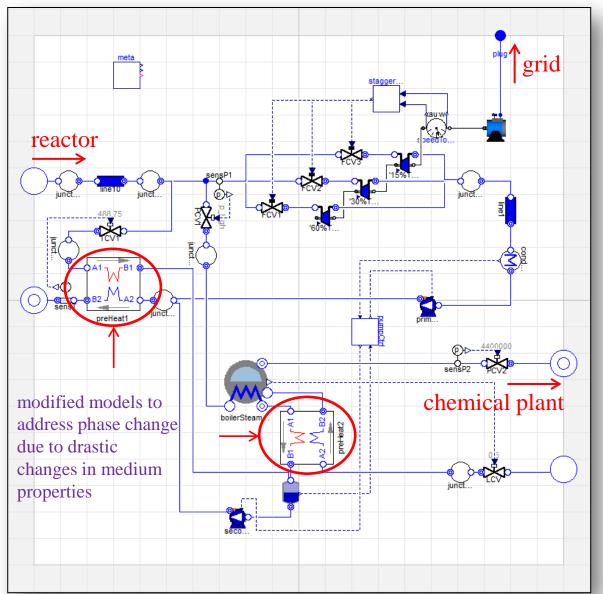


- Constant heat source
- Next: exploring partial load-following



# Power Subsystem

- Two loops
  - Three turbines
  - Secondary boiler
- Turbines have priority
  - 3 coaxial turbines
  - Sized as 60%, 30%, 15% of nominal
- Coordinated two-pump control
  - Maintain 311°C at reactor outlet by varying flow rates

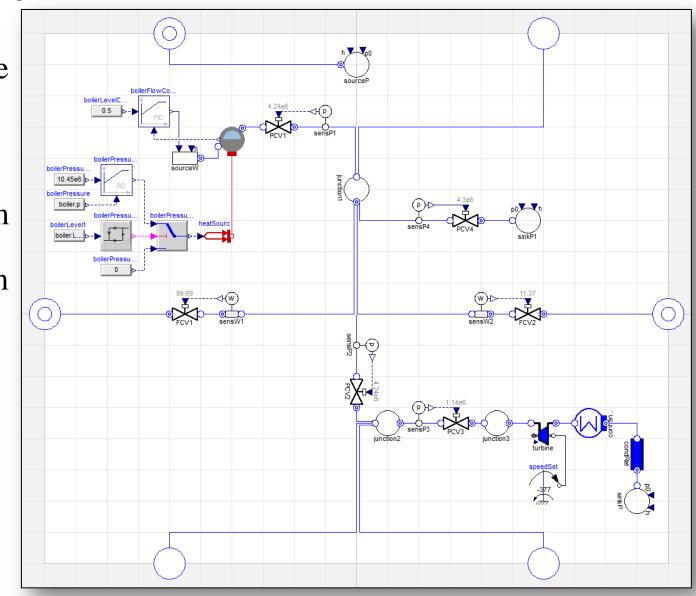


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# **Power Control for Chemical Plant**

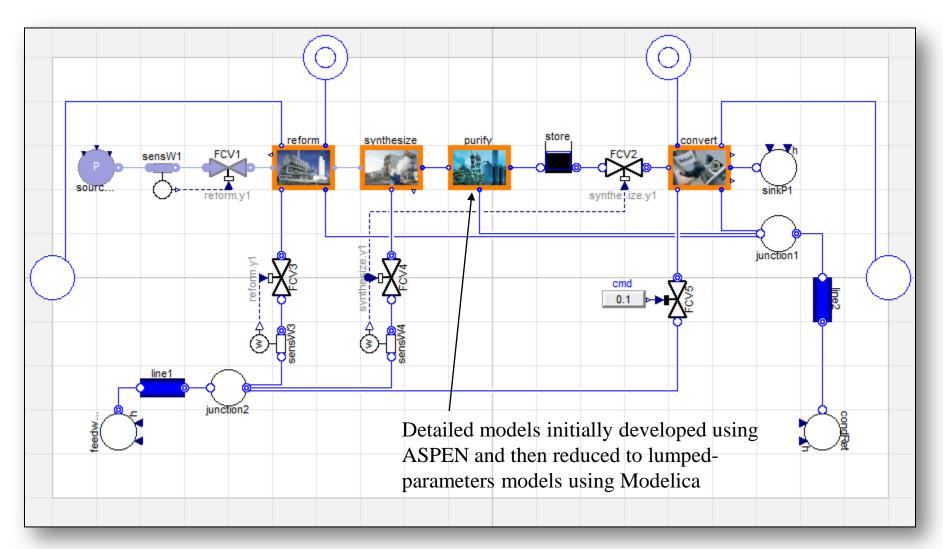
- Low-pressure and high-pressure steam headers
- Utility boiler compensates for variation in steam coming from Power Subsystem
- Waste heat recovered in secondary turbines





### **Chemical Plant**

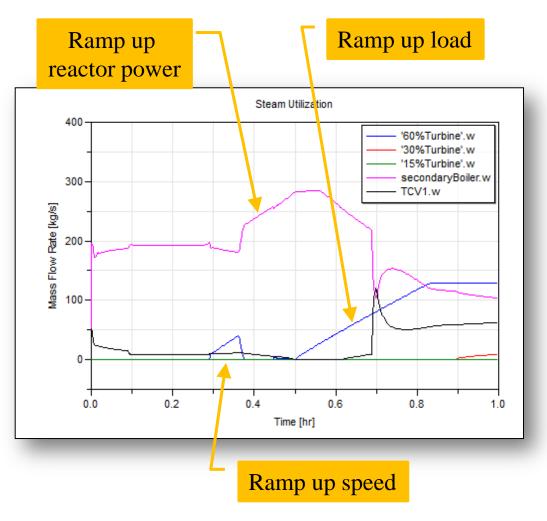
#### • Process-based reduced-order models (ROM)





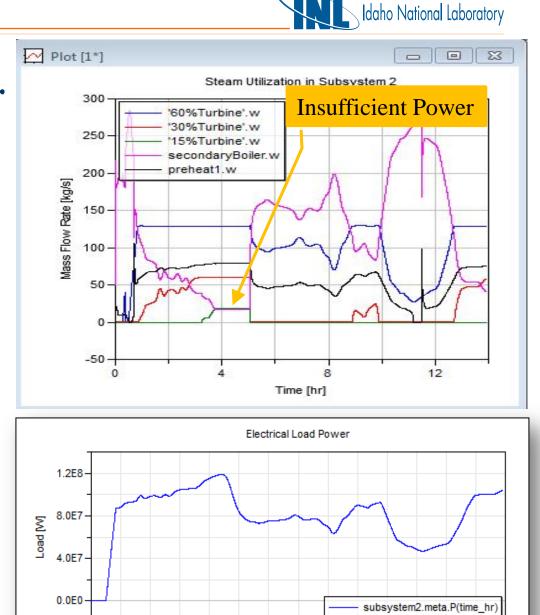
#### Power Subsystem Start-up / Shutdown

- Three P, T (h)
  - Reactor inlet
  - Reactor outlet
  - Condenser inlet
- Nominal RPM for both pumps
- Startup sequence
  - Start turbines idle at 0 RPM
  - Wait for transients to die out
  - Ramp up turbine to 60Hz
  - Ramp up reactor power
  - Ramp up load to nominal at 60Hz



#### Compensating for Variation in Wind Power

- Three turbines turn on or off to produce desired electrical power
- Insufficient power could be covered using grid-battery
- Excess steam is diverted to secondary boiler and on to chemical plant



5

Time [hr]

10

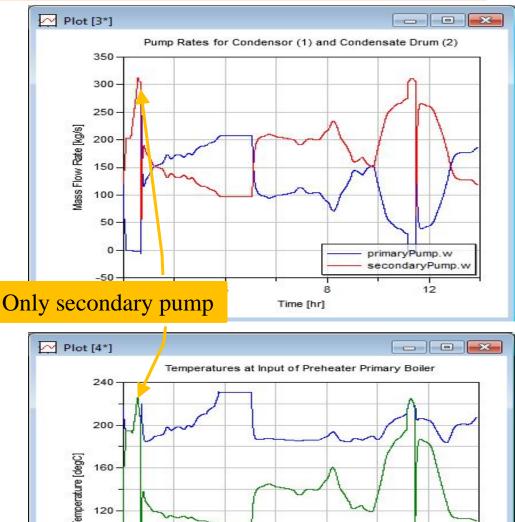


condensateDrum.T condenser.T preHeat1.infl.T

12

# *Controlling the Pumps*

- Coordinated pump control
  - Maintain 311°C at reactor outlet by varying flow rates
- Variable speed pump control
- Total mass flow divided proportional to level of drums
- Temperature of the input flow to pre-heater of primary boiler varies significantly depending on which pump the feed comes from



Time [hr]

120

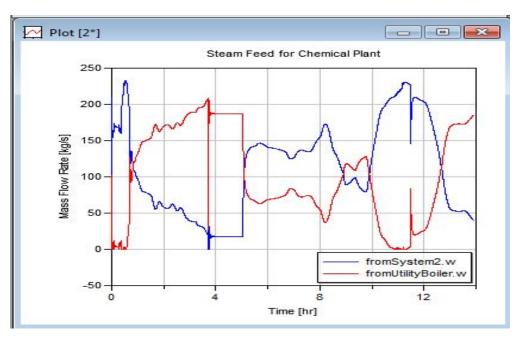
80

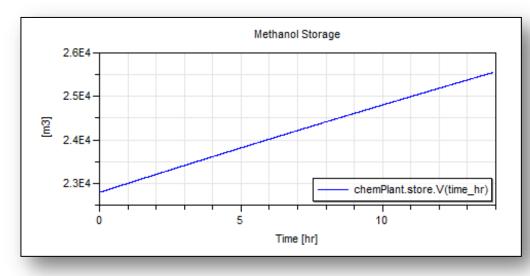
40



#### **Chemical Plant**

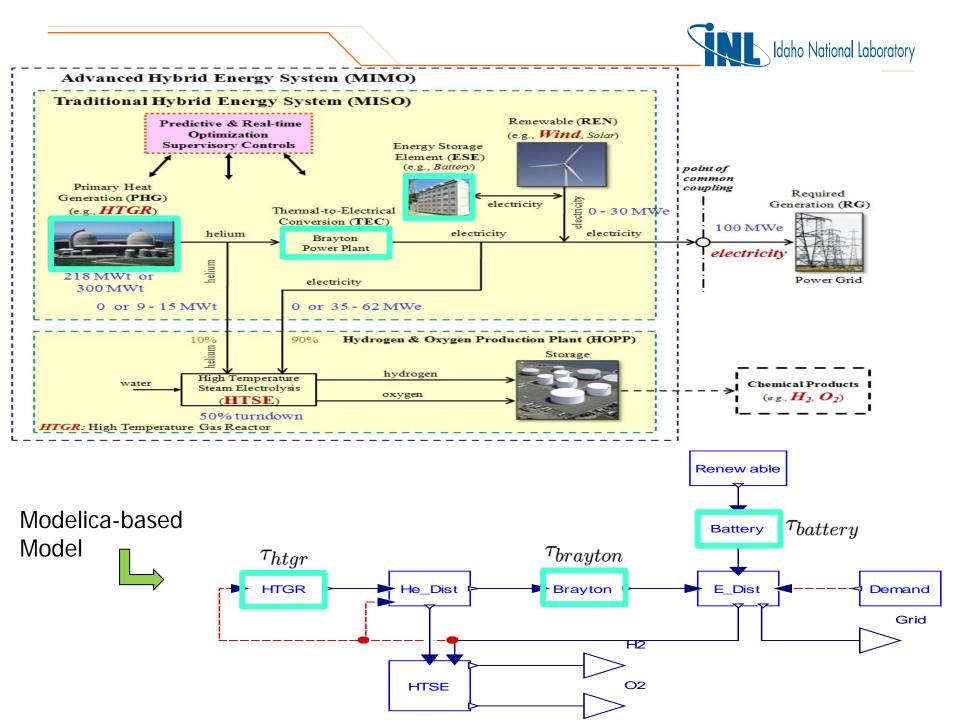
- Utility boiler compensates for variation in steam coming from Power Subsystem
- Chemical plant currently runs in steady state
- Methanol stored increases at constant rate







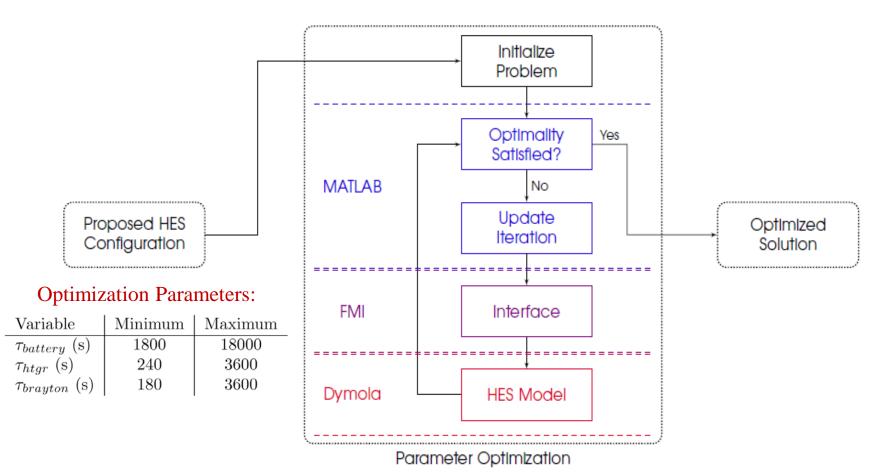
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#### **Computational Framework**

- Three major software tools comprise the present framework:
  - Dymola platform for Modelica-base HES model;
  - MATLAB platform for numerical optimizer;
  - FMI interface for Dymola and MATLAB to execute HES simulations.



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# **Optimization Methodology**

• General optimization problem minimizes objective function for certain constraints:

 $\begin{array}{l} \text{minimize } f(x), f \colon \Re^n \to \Re \\ \text{subject to} \begin{cases} x_{lower} \leq x \leq x_{upper} \\ c_k(x) \leq 0, k = 1, \dots, m \\ \hat{c}_j(x) = 0, j = 1, \dots, \hat{m} \end{cases} \end{array}$ 

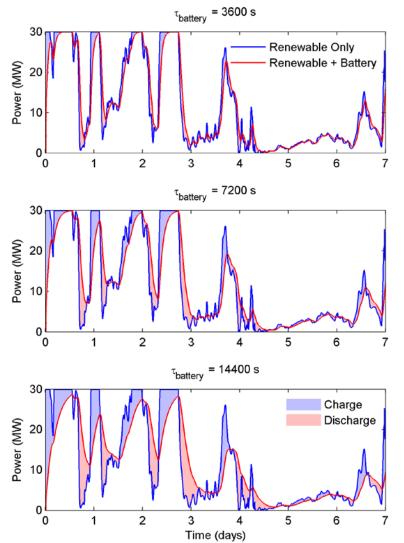
- Many optimizers for solving this problem exist; we use the Nelder-Mead simplex method (gradient-free thus suitable for noisy functions).
- Objective function is defined as the total variability in HTSE electrical power  $P_{htse}^{e}(t):$   $f(x) = \int_{0}^{t_{f}} |P_{htse}^{e}(t) - \bar{P}_{htse}^{e}|dt$
- Constraints are enforced by modifying objective function with a quadratic penalty function:

$$\varphi(x) = f(x) + p(x) = f(x) + \sum_{i=1}^{m+\widehat{m}} b_i \max(0, c_i)^2$$



# Effect of Battery Size

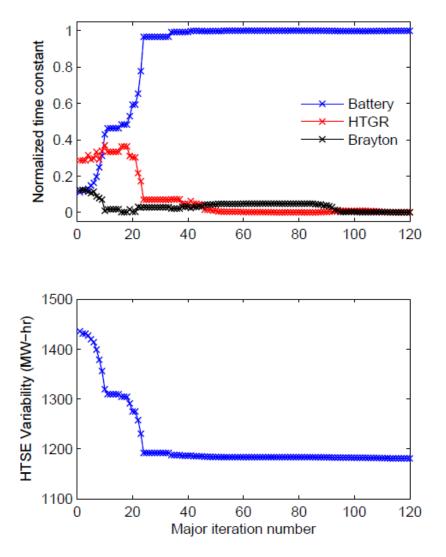
- Shaded area is electrical energy storage associated with the battery.
- Battery sizing and operation is a complex problem involving competing objectives
  - less battery storage leads to greater electrical variability (leading to higher operational cost of the system);
  - more battery storage smoothes out electrical variability from renewables (leading to higher capital cost of the system).



# **Unconstrained Optimization Results**

- Without constraints, time constants converge to bounds:
  - larger battery ( $\tau_{battery} = 18000$  s) smoothes out renewable variability;
  - fastest reactor ( $\tau_{htgr} = 240$  s) and power cycle ( $\tau_{brayton} = 180$  s) aid in load following.
- Constraints need to be included to properly account for negative impacts of larger battery and faster reactor/power cycle (i.e., higher cost).
- Time constants normalized based on upper and lower bounds:

$$\tau^* = \frac{\tau - \tau_{\min}}{\tau_{\max} - \tau_{\min}}$$



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# **Constrained Optimization Results**

• Linear cost function used as inequality constraint:

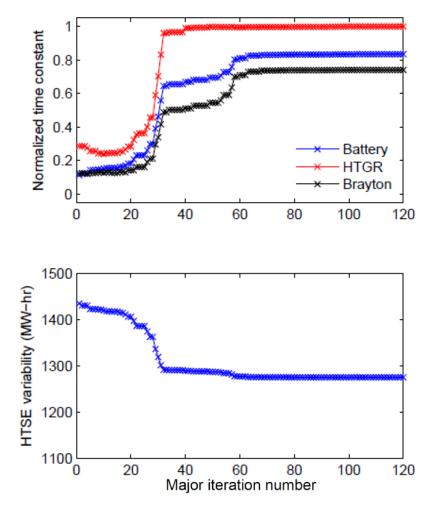
$$c_1(x) = k_1 \tau_{battery} - k_2 \tau_{htgr} - k_3 \tau_{brayton} \le 0$$

• Two nonlinear constraints restrict the relative time constants of HTGR and Brayton cycle:

$$c_2 = \frac{\tau_{htgr}}{\tau_{brayton}} - 2 \le 0$$

$$c_3 = \frac{\tau_{brayton}}{\tau_{htgr}} - 2 \le 0$$

- Constraint forces optimizer to compromise between competing effects of performance and cost.
- One time constant converges to the maximum value (HTGR); others to optimal intermediate values



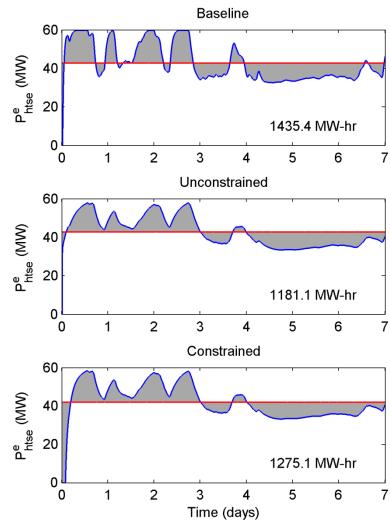


## **Optimization Summary**

	Baseline	Unconstrained	Constrained
$\tau_{battery}$ (s)	3600	18000	15311
$\tau_{htgr}$ (s)	1200	240	3600
$\tau_{brayton}$ (s)	600	180	2712
f(x) (MW-hr)	1435.4	1181.1	1275.1

- Variability in HTSE electrical power is reduced by 18% and 11% using unconstrained and constrained optimization, respectively.
- Shaded area graphically illustrates effect of dynamic optimization:
  - HTSE operation is smoothed out to reduce variability;
  - primary effect of constraints is slower initial ramping of HTSE;

Variable	Minimum	Maximum
$\tau_{battery}$ (s)	1800	18000
$\tau_{htgr}$ (s)	240	3600
$\tau_{brayton}$ (s)	180	3600



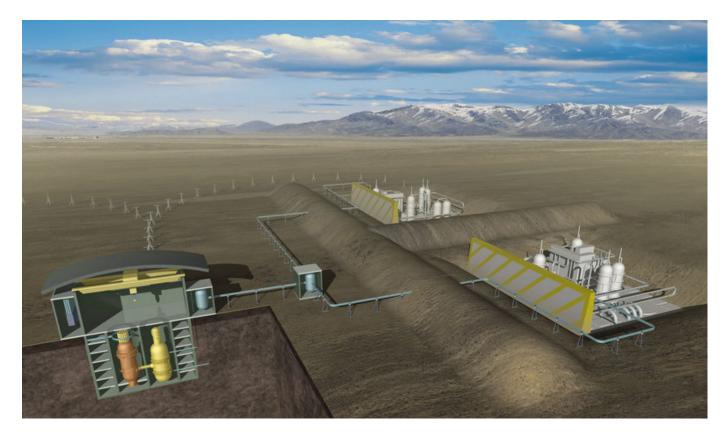


# **Conclusions & On-going Directions**

- Complex dynamics occur due to:
  - transient physical behavior, controller interactions, renewables variability & uncertainty
- Cannot be adequately analyzed using steady-state tools (e.g., in Aspen)
- Dynamic M&S crucial for design and operation of Hybrid Energy Systems
- Development of additional M&S capabilities
  - RTDS & hardware co-simulation connectivity
  - wind / solar application models
  - chemical process models (e.g., high temperature steam electrolysis, HTSE)
  - SMR models
  - Robust models for predicting anomalous operating conditions
- Development of design optimization techniques, tools & technologies
- Development of hardware capabilities (e.g., thermal loop for HiL demo)
- Development of predictive (look-ahead) supervisory controls & real-time optimization for optimized operations and economics
- Detailed analysis of dynamics of tightly-coupled power generation -process systems and design of systems to moderate the extremes



#### **Questions ?**



Conceptual nuclear-driven complex for power, hydrogen, and synfuel production